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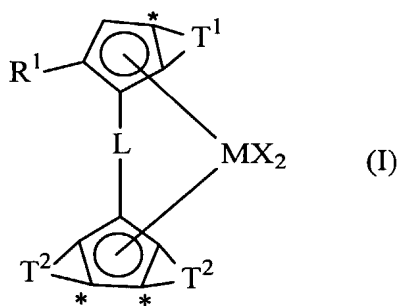
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(54) Title: PROCESS FOR POLYMERIZING 1-HEXENE OR HIGHER ALPHA-OLEFINS



(57) Abstract: A process for preparing a polymer containing derived units of one or more alpha olefins of formula $\text{CH}_2=\text{CHW}$ wherein W is a $\text{C}_3\text{-C}_{10}$ hydrocarbon radical and optionally from 0 to 81% by mol of derived units of propylene or 1-butene, comprising contacting under polymerization conditions one or more alpha olefins of formula $\text{CH}_2=\text{CHW}$ and optionally propylene or 1-butene in the presence of a catalyst system obtainable by contacting: a) a metallocene compound of formula (I), wherein M, X, L, T^1 , T^2 , T^3 and R^1 are described in the text; and (b) an alumoxane or a compound capable of forming an alkyl metallocene cation.



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Process for polymerizing 1-hexene or higher alpha-olefins

The present invention relates to a process for obtaining a polymer comprising 1-hexene or higher alpha-olefins derived units, by using a specific class of metallocene compounds, that allows to obtain polymers having high molecular weight in high yields.

Metallocene compounds are well known catalyst components for the polymerization of alpha-olefins. However they are mainly used for the (co)polymerization of ethylene, propylene and 1-butene. Polymerization of 1-hexene and higher alpha olefins by using metallocene catalyst components is discussed in some papers. For example US 6,566,544 discloses in table 10 the polymerization of 1-hexene by using $\text{Ind}_2\text{ZrMe}_2$ and bis(2-phenylindenyl)zirconium dimethyl. The molecular weight of the obtained polymers are quite low. In Macromol. Chem.Phys. 200, 1208-1219 (1999), 1-hexene is polymerized in the presence of $\text{iPr}(\text{CpFlu})\text{ZrCl}_2$. The polymer has a syndiotactic structure and the molecular mass of the polymer obtained is close to 20000 g mol^{-1} . In Journal of Polymer Science: Part A: Polymer Chemistry, Vol 37, 283-292 (1999) a series of metallocene compounds have been tested in 1-hexene polymerization. *Rac*- $[\text{Me}_2\text{Ge}(\eta^5\text{-C}_5\text{H-2,3,5-Me}_3)\text{MCl}_2$ (M = Zr or Hf) allows to obtain 1-hexene polymers having a very high molecular weight. However the drawback of this compound is that it is necessary to separate the racemic from the meso form, this makes the synthesis of such compound much more difficult and expensive than the metallocene compound of the present invention. In the same article is also shown that isopropyliden(9-fluorenyl)(cyclopentadienyl)zirconium dichloride produces 1-hexene polymer having very low molecular weight, with respect to the other compounds tested. The behaviour of isopropyliden(9-fluorenyl)(cyclopentadienyl)zirconium dichloride is confirmed in Macromol. Mater. Eng. 2001, 286, 480-487. In this paper the molecular weight (M_w) of 1-hexene polymer obtained by using said compound is about 45000.

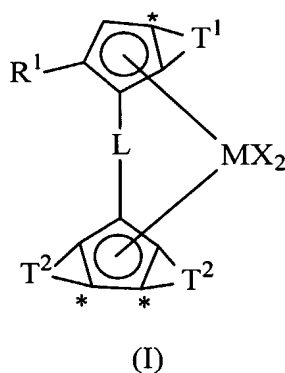
WO 01/46278 relates to a polymerization process for producing a copolymer containing from 60 to 94% mol of alpha olefins having from 3 to 6 carbon atoms, and from 6 to 40% mol of alpha olefins having at least one carbon atom more than the first one. In the examples propylene is copolymerized with 1-hexene. These copolymers are obtained with a metallocene compound different from that one used in the present invention, moreover the molecular weight of the obtained copolymers can still be improved. Finally the present invention is directed to a copolymer that contains a smaller amount of propylene or 1-butene.

In Macromol. Chem.Phys. 197, 563-573 (1996) are described a series of hexene propylene copolymers having various content of comonomer from 0 to 100% by mol. The copolymers are obtained by using $\text{Et(Ind)}_2\text{HfCl}_2$ and both the yields and the molecular weight of the obtained polymers can be further improved.

Thus there is still the need to find a class of metallocene compounds easy to prepare and without the drawback to separate the racemic from the meso form able to give 1-hexene or higher alpha-olefins (co)polymers having an high molecular weight in high yields.

An object of the present invention is a process for preparing a polymer containing derived units of one or more alpha olefins of formula $\text{CH}_2=\text{CHW}$ wherein W is a $\text{C}_3\text{-C}_{10}$ hydrocarbon radical and optionally from 0 to 81% by mol; preferably from 0 to 70% by mol, more preferably from 0 to 59% by mol, of derived units of propylene or 1-butene, comprising contacting under polymerization conditions one or more alpha olefins of formula $\text{CH}_2=\text{CHW}$ and optionally propylene or 1-butene in the presence of a catalyst system obtainable by contacting:

a) a metallocene compound of formula (I)



wherein:

M is an atom of a transition metal selected from those belonging to group 3, 4, or to the lanthanide or actinide groups in the Periodic Table of the Elements; preferably M is zirconium titanium or hafnium;

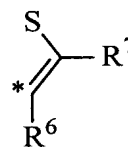
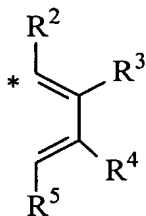
X, same or different, is a hydrogen atom, a halogen atom, or a R, OR, OSO_2CF_3 , OCOR, SR, NR_2 or PR_2 group, wherein R is a are linear or branched, cyclic or acyclic, $\text{C}_1\text{-C}_{40}$ -alkyl, $\text{C}_2\text{-C}_{40}$ alkenyl, $\text{C}_2\text{-C}_{40}$ alkynyl, $\text{C}_6\text{-C}_{40}$ -aryl, $\text{C}_7\text{-C}_{40}$ -alkylaryl or $\text{C}_7\text{-C}_{40}$ -arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or two X can optionally form a substituted or unsubstituted butadienyl radical or a $\text{OR}'\text{O}$ group wherein R' is a divalent radical

selected from C₁-C₄₀ alkylidene, C₆-C₄₀ arylidene, C₇-C₄₀ alkylarylidene and C₇-C₄₀ arylalkylidene radicals; preferably X is a hydrogen atom, a halogen atom or a R group; more preferably X is chlorine or a C₁-C₁₀-alkyl radical; such as methyl, or ethyl radicals;

L is a divalent C₁-C₄₀ hydrocarbon radical optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements or a divalent silylene radical containing up to 5 silicon atom; preferably L is a divalent bridging group selected from C₁-C₄₀ alkylidene, C₃-C₄₀ cycloalkylidene, C₆-C₄₀ arylidene, C₇-C₄₀ alkylarylidene, or C₇-C₄₀ arylalkylidene radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements, and silylene radical containing up to 5 silicon atoms such as SiMe₂, SiPh₂; preferably L is a group (Z(R''))₂)_n wherein Z is a carbon or a silicon atom, n is 1 or 2 and R'' is a C₁-C₂₀ hydrocarbon radical optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; preferably R'' is a linear or branched, cyclic or acyclic, C₁-C₂₀-alkyl, C₂-C₂₀ alkenyl, C₂-C₂₀ alkynyl, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀-arylalkyl radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; more preferably the group (Z(R''))₂)_n is Si(CH₃)₂, SiPh₂, SiPhMe, SiMe(SiMe₃), CH₂, (CH₂)₂, and C(CH₃)₂;

R¹, is a hydrogen atom, or a C₁-C₄₀ hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; Preferably R¹ is a hydrogen atom or a linear or branched, cyclic or acyclic, C₁-C₄₀-alkyl, C₂-C₄₀ alkenyl, C₂-C₄₀ alkynyl, C₆-C₄₀-aryl, C₇-C₄₀-alkylaryl or C₇-C₄₀-arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; more preferably R¹ is linear or branched, saturated or unsaturated C₁-C₂₀-alkyl radicals, optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; even more preferably R¹ is a C₁-C₁₀-alkyl radical such as a methyl, or ethyl radical;

T¹ is a moiety of formula (IIa) or (IIb):



(IIa)

(IIb)

wherein the atom marked with the symbol * bonds the atom marked with the same symbol in the compound of formula (I);

R^2 , R^3 , R^4 and R^5 , equal to or different from each other, are hydrogen atoms, or C_1 - C_{40} hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or two adjacent R^2 , R^3 , R^4 and R^5 can optionally form a saturated or unsaturated, 5 or 6 membered rings, said ring can bear C_1 - C_{20} alkyl radicals as substituents; Preferably R^2 , R^3 , R^4 and R^5 are hydrogen atoms or linear or branched, cyclic or acyclic, C_1 - C_{40} -alkyl, C_2 - C_{40} alkenyl, C_2 - C_{40} alkynyl, C_6 - C_{40} -aryl, C_7 - C_{40} -alkylaryl or C_7 - C_{40} -arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements;

R^2 is preferably a linear or branched, saturated or unsaturated C_1 - C_{20} -alkyl radical, optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; preferably R^2 is a C_1 - C_{10} -alkyl radical; more preferably R^2 is a methyl, ethyl or isopropyl radical;

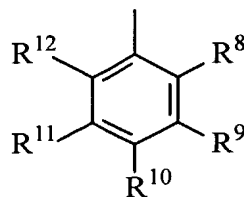
R^4 is preferably a hydrogen atom or a C_1 - C_{10} -alkyl radical such as a methyl, ethyl or isopropyl radical;

R^5 is preferably a hydrogen atom or linear or branched, saturated or unsaturated C_1 - C_{20} -alkyl radical, optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; preferably a C_1 - C_{10} -alkyl radical; more preferably R^5 is a methyl or ethyl radical;

R^6 and R^7 , equal to or different from each other, are hydrogen atoms or C_1 - C_{40} hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or R^6 and R^7 can optionally form a saturated or unsaturated, 5 or 6 membered rings, said ring can bear C_1 - C_{20} alkyl radicals as substituents; preferably R^6 and R^7 are hydrogen atoms or linear or branched, cyclic or acyclic, C_1 - C_{40} -alkyl, C_2 - C_{40} alkenyl, C_2 - C_{40} alkynyl, C_6 - C_{40} -aryl, C_7 - C_{40} -alkylaryl or C_7 - C_{40} -arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements;

preferably R^7 is a hydrogen atom or a linear or branched, cyclic or acyclic C_1 - C_{20} -alkyl radical; more preferably R^7 is a methyl or ethyl radical;

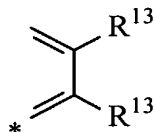
preferably R^6 is a C_1 - C_{40} -alkyl, C_6 - C_{40} -aryl or a C_7 - C_{40} -arylalkyl; more preferably R^6 is a group of formula (III)



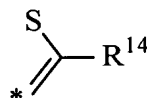
(III)

wherein R⁸, R⁹, R¹⁰, R¹¹ and R¹², equal to or different from each other, are hydrogen atoms or C₁-C₂₀ hydrocarbon radicals; preferably R⁸, R⁹, R¹⁰, R¹¹ and R¹² are hydrogen atoms or linear or branched, cyclic or acyclic, C₁-C₂₀-alkyl, C₂-C₂₀ alkenyl, C₂-C₂₀ alkynyl, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀-arylalkyl radicals; preferably R⁸, and R¹¹ are a hydrogen atoms; R⁹, R¹⁰ and R¹² are preferably hydrogen atoms or linear or branched, cyclic or acyclic, C₁-C₁₀-alkyl radicals;

T², equal to or different from each other, are moieties of formula (IIc) or (IId):



(IIc)



(IId)

wherein the atom marked with the symbol * bonds the atom marked with the same symbol in the compound of formula (I);

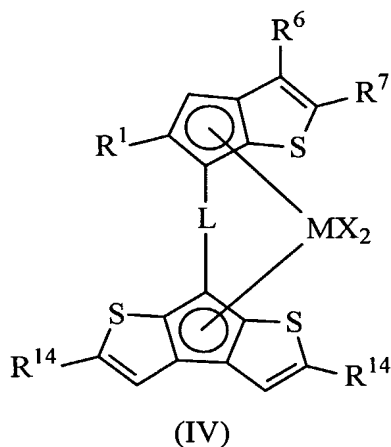
R¹³, equal to or different from each other, are hydrogen atoms or C₁-C₄₀ hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or two R¹³ can optionally form a saturated or unsaturated, 5 or 6 membered rings, said ring can bear C₁-C₂₀ alkyl radicals as substituents; preferably R¹³ are hydrogen atoms or linear or branched, cyclic or acyclic, C₁-C₄₀-alkyl, C₂-C₄₀ alkenyl, C₂-C₄₀ alkynyl, C₆-C₄₀-aryl, C₇-C₄₀-alkylaryl or C₇-C₄₀-arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; more preferably R¹³ are a hydrogen atoms or linear or branched, C₁-C₂₀-alkyl radicals;

R¹⁴, equal to or different from each other, are hydrogen atoms or C₁-C₄₀ hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; preferably R¹⁴ are linear or branched, cyclic or acyclic, C₁-C₄₀-alkyl, C₂-C₄₀ alkenyl, C₂-C₄₀ alkynyl, C₆-C₄₀-aryl, C₇-C₄₀-alkylaryl or C₇-C₄₀-arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17

of the Periodic Table of the Elements; more preferably R^{14} are linear or branched, C_1 - C_{20} -alkyl radicals;

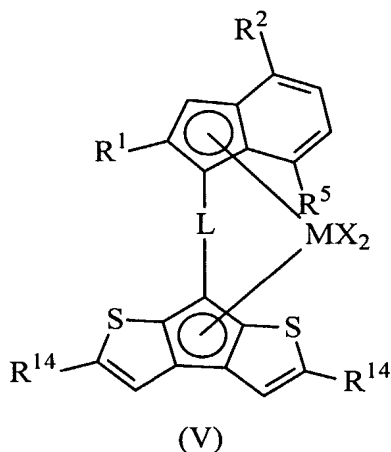
- (b) an alumoxane or a compound capable of forming an alkyl metallocene cation; and optionally
- (c) an organo aluminum compound.

In one embodiment the compound of formula (I) has the following formula (IV)



wherein M, X, L, R^1 , R^6 , R^7 , and R^{14} are described above.

In a further alternative embodiment the compound of formula (I) has the following formula (V)



wherein M, X, L, R^1 , R^2 , R^5 and R^{14} are described above.

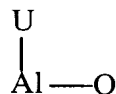
compounds of formula (I) are well known in the art, they can be prepared for example as described in WO 01/47939 or EP 707 016.

Alumoxanes used as component b) can be obtained by reacting water with an organo-aluminium compound of formula H_jAlU_{3-j} or $H_jAl_2U_{6-j}$, where the U substituents, same or different, are hydrogen atoms, halogen atoms, C_1 - C_{20} -alkyl, C_3 - C_{20} -cyclalkyl, C_6 - C_{20} -aryl, C_7 -

C₂₀-alkylaryl or C₇-C₂₀-arylalkyl radicals, optionally containing silicon or germanium atoms, with the proviso that at least one U is different from halogen, and j ranges from 0 to 1, being also a non-integer number. In this reaction the molar ratio of Al/water is preferably comprised between 1:1 and 100:1.

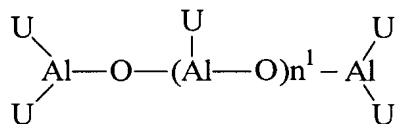
Alumoxanes used as component b) can be obtained by reacting water with an organo-aluminium compound of formula H_jAlU_{3-j} or H_jAl₂U_{6-j}, where the U substituents, same or different, are hydrogen atoms, halogen atoms, C₁-C₂₀-alkyl, C₃-C₂₀-cyclalkyl, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀-arylalkyl radicals, optionally containing silicon or germanium atoms, with the proviso that at least one U is different from halogen, and j ranges from 0 to 1, being also a non-integer number. In this reaction the molar ratio of Al/water is preferably comprised between 1:1 and 100:1.

The alumoxanes used in the process according to the invention are considered to be linear, branched or cyclic compounds containing at least one group of the type:

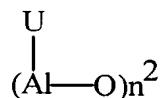


wherein the substituents U, same or different, are defined above.

In particular, alumoxanes of the formula:



can be used in the case of linear compounds, wherein n¹ is 0 or an integer of from 1 to 40 and the substituents U are defined as above; or alumoxanes of the formula:



can be used in the case of cyclic compounds, wherein n² is an integer from 2 to 40 and the U substituents are defined as above.

Examples of alumoxanes suitable for use according to the present invention are methylalumoxane (MAO), tetra-(isobutyl)alumoxane (TIBAO), tetra-(2,4,4-trimethylpentyl)alumoxane (TIOAO), tetra-(2,3-dimethylbutyl)alumoxane (TDMBAO) and tetra-(2,3,3-trimethylbutyl)alumoxane (TTMBAO).

Particularly interesting cocatalysts are those described in WO 99/21899 and in WO01/21674 in which the alkyl and aryl groups have specific branched patterns.

Non-limiting examples of aluminium compounds that can be reacted with water to give suitable alumoxanes (b), described in WO 99/21899 and WO01/21674, are:

tris(2,3,3-trimethyl-butyl)aluminium, tris(2,3-dimethyl-hexyl)aluminium, tris(2,3-dimethyl-butyl)aluminium, tris(2,3-dimethyl-pentyl)aluminium, tris(2,3-dimethyl-heptyl)aluminium, tris(2-methyl-3-ethyl-pentyl)aluminium, tris(2-methyl-3-ethyl-hexyl)aluminium, tris(2-methyl-3-ethyl-heptyl)aluminium, tris(2-methyl-3-propyl-hexyl)aluminium, tris(2-ethyl-3-methyl-butyl)aluminium, tris(2-ethyl-3-methyl-pentyl)aluminium, tris(2,3-diethyl-pentyl)aluminium, tris(2-propyl-3-methyl-butyl)aluminium, tris(2-isopropyl-3-methyl-butyl)aluminium, tris(2-isobutyl-3-methyl-pentyl)aluminium, tris(2,3,3-trimethyl-pentyl)aluminium, tris(2,3,3-trimethyl-hexyl)aluminium, tris(2-ethyl-3,3-dimethyl-butyl)aluminium, tris(2-ethyl-3,3-dimethyl-pentyl)aluminium, tris(2-isopropyl-3,3-dimethyl-butyl)aluminium, tris(2-trimethylsilyl-propyl)aluminium, tris(2-methyl-3-phenyl-butyl)aluminium, tris(2-ethyl-3-phenyl-butyl)aluminium, tris(2,3-dimethyl-3-phenyl-butyl)aluminium, tris(2-phenyl-propyl)aluminium, tris[2-(4-fluoro-phenyl)-propyl]aluminium, tris[2-(4-chloro-phenyl)-propyl]aluminium, tris[2-(3-isopropyl-phenyl)-propyl]aluminium, tris(2-phenyl-butyl)aluminium, tris(3-methyl-2-phenyl-butyl)aluminium, tris(2-phenyl-pentyl)aluminium, tris[2-(pentafluorophenyl)-propyl]aluminium, tris[2,2-diphenyl-ethyl]aluminium and tris[2-phenyl-2-methyl-propyl]aluminium, as well as the corresponding compounds wherein one of the hydrocarbyl groups is replaced with a hydrogen atom, and those wherein one or two of the hydrocarbyl groups are replaced with an isobutyl group.

Amongst the above aluminium compounds, trimethylaluminium (TMA), triisobutylaluminium (TIBA), tris(2,4,4-trimethyl-pentyl)aluminium (TIOA), tris(2,3-dimethylbutyl)aluminium (TDMBA) and tris(2,3,3-trimethylbutyl)aluminium (TTMBA) are preferred.

Non-limiting examples of compounds able to form an alkylmetallocene cation are compounds of formula D^+E^- , wherein D^+ is a Brønsted acid, able to donate a proton and to react irreversibly with a substituent X of the metallocene of formula (I) and E^- is a compatible anion, which is able to stabilize the active catalytic species originating from the reaction of the two compounds, and which is sufficiently labile to be removed by an olefinic monomer. Preferably, the anion E^- comprises one or more boron atoms. More preferably, the anion E^- is an anion of the formula $BAr_4^{(-)}$, wherein the substituents Ar which can be identical or different are aryl radicals such as phenyl, pentafluorophenyl or bis(trifluoromethyl)phenyl.

Tetrakis-pentafluorophenyl borate is particularly preferred compound, as described in WO 91/02012. Moreover, compounds of formula BAr_3 can be conveniently used. Compounds of this type are described, for example, in the International patent application WO 92/00333. Other examples of compounds able to form an alkylmetallocene cation are compounds of formula BAr_3P wherein P is a substituted or unsubstituted pyrrol radical. These compounds are described in WO01/62764. Compounds containing boron atoms can be conveniently supported according to the description of DE-A-19962814 and DE-A-19962910. All these compounds containing boron atoms can be used in a molar ratio between boron and the metal of the metallocene comprised between about 1:1 and about 10:1; preferably 1:1 and 2.1; more preferably about 1:1.

Non limiting examples of compounds of formula D^+E^- are:

Triethylammoniumtetra(phenyl)borate,
Tributylammoniumtetra(phenyl)borate,
Trimethylammoniumtetra(tolyl)borate,
Tributylammoniumtetra(tolyl)borate,
Tributylammoniumtetra(pentafluorophenyl)borate,
Tributylammoniumtetra(pentafluorophenyl)aluminate,
Tripropylammoniumtetra(dimethylphenyl)borate,
Tributylammoniumtetra(trifluoromethylphenyl)borate,
Tributylammoniumtetra(4-fluorophenyl)borate,
N,N-Dimethylbenzylammonium-tetrakis(pentafluorophenyl)borate,
N,N-Dimethylhexylammonium-tetrakis(pentafluorophenyl)borate,
N,N-Dimethylaniliniumtetra(phenyl)borate,
N,N-Diethylaniliniumtetra(phenyl)borate,
N,N-Dimethylaniliniumtetrakis(pentafluorophenyl)borate,
N,N-Dimethylaniliniumtetrakis(pentafluorophenyl)aluminate,
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Triphenylphosphoniumtetrakis(phenyl)borate,
Triethylphosphoniumtetrakis(phenyl)borate,
Diphenylphosphoniumtetrakis(phenyl)borate,

Tri(methylphenyl)phosphoniumtetrakis(phenyl)borate,
 Tri(dimethylphenyl)phosphoniumtetrakis(phenyl)borate,
 Triphenylcarbeniumtetrakis(pentafluorophenyl)borate,
 Triphenylcarbeniumtetrakis(pentafluorophenyl)aluminate,
 Triphenylcarbeniumtetrakis(phenyl)aluminate,
 Ferroceniumtetrakis(pentafluorophenyl)borate,
 Ferroceniumtetrakis(pentafluorophenyl)aluminate.
 Triphenylcarbeniumtetrakis(pentafluorophenyl)borate, and
 N,N-Dimethylaniliniumtetrakis(pentafluorophenyl)borate.

Organic aluminum compounds used as compound iii) are those of formula H_jAlU_{3-j} or $H_jAl_2U_{6-j}$ as described above.

The polymerization process of the present invention can be carried out in liquid phase, optionally in the presence of an inert hydrocarbon solvent. Said hydrocarbon solvent can be either aromatic (such as toluene) or aliphatic (such as propane, hexane, heptane, isobutane, cyclohexane and 2,2,4-trimethylpentane). Preferably, the polymerization process of the present invention is carried out by using the alpha olefin of formula $CH_2=CHW$ wherein W is a C_3 - C_{10} hydrocarbon radical such as 1-hexene or 1-octene as polymerization medium, i.e. the same olefin that is going to be polymerized for example 1-hexene is used as polymerization medium when a 1-hexene-based polymer is the wished polymer.

The polymerization temperature preferably ranges from 0°C to 250°C; more preferably it is comprised between 20°C and 150°C and, more particularly the polymerization temperature is between 40°C and 90°C;

The molecular weight distribution can be varied by using mixtures of different metallocene compounds or by carrying out the polymerization in several stages which differ as to the polymerization temperature and/or the concentrations of the molecular weight regulators and/or the monomers concentration. Moreover by carrying out the polymerization process by using a combination of two different metallocene compounds of formula (I) a polymer endowed with a broad melting is produced.

With the process of the present invention isotactic polymers endowed with high molecular weights can be obtained in high yields.

With the process of the present invention polymers containing derived units of one or more alpha olefins of formula $CH_2=CHW$ wherein W is a C_3 - C_{10} hydrocarbon radical and optionally from 0 to 81% by mol of derived units of propylene or 1-butene can be

obtained. Examples of alpha olefins of formula $\text{CH}_2=\text{CHW}$ are 1-pentene; 1-hexene; 1-octene and 1-decene. Preferably 1-hexene and 1-octene are used; more preferably 1-hexene is used.

When said alpha olefins of formula $\text{CH}_2=\text{CHW}$ are copolymerized with propylene or 1-butene preferably the obtained copolymer has a content of derived units of propylene or 1-butene ranging from 0.1% by mol to 59% by mol; more preferably the content of propylene or 1-butene ranges from 10% by mol to 50% by mol, even more preferably it ranges from 19% by mol to 40% by mol.

The obtained copolymer is endowed with the following properties:

- i) intrinsic viscosity IV measured in tetrahydronaphtalene (THN) at 135°C higher than 0.90 dl/g; preferably higher than 1.20 dl/g; more preferably higher than 1.30 dl/g; even more preferably higher than 1.80 dl/g;
- ii) distribution of molecular weight M_w/M_n lower than 3; preferably lower than 2.5; and
- iii) no enthalpy of fusion detectable at a differential scanning calorimeter (DSC) wherein the DSC measurement is carried out as described below.

Preferably in said copolymers the alpha olefin of formula $\text{CH}_2=\text{CHW}$ is 1-hexene or 1-octene.

The copolymers, other than the above properties, are further endowed with a very low Shore A (measured according to ISO 868), in particular the shore A is lower than 30; preferably lower than 25; more preferably lower than 20; and furthermore the tensile modulus is lower than 20 MPa (measured according to ASTM 5026,4092 e 4065); preferably lower than 15MPa; more preferably lower than 11 MPa.

A further preferred range of content of derived units of propylene and 1-butene is from 19% by mol to 59% by mol; even more preferably from 30% by mol to 59% by mol.

The process of the present invention is particularly suitable for preparing homopolymers of alpha olefins of formula $\text{CH}_2=\text{CHW}$ wherein W is a $\text{C}_3\text{-C}_{10}$ hydrocarbon radical, in particular homopolymers of 1-hexene or 1-octene; preferably homopolymer of 1-hexene are produced.

The homopolymer prepared according to the present invention can be used for application known in the art such as masterbatches or in adhesive formulations.

Even if the homopolymer of the present invention are not exemplified, their preparation can be easily achieved by the skilled man once it is know the process for preparing the

copolymers. In fact it is sufficient to avoid to add the comonomer in the processes exemplified above for obtaining the wished homopolymer.

The copolymers obtainable with the process of the present invention described above, can have the same uses of the homopolymer and furthermore they can be used as compatibilizer. For example they can improve the dispersion of a rubber phase in an crystalline matrix, due to the presence of the comonomer that help to compatibilize the two phases, so that a material having an improved izod impact value can be obtained.

The following examples are given to illustrate and not to limit the invention.

EXAMPLES

GENERAL PROCEDURES AND CHARACTERIZATIONS

All chemicals were handled under nitrogen using standard Schlenk techniques.

Methylalumoxane (MAO) was received from Albemarle as a 30% wt/vol toluene solution and used as such.

Pure triisobutylaluminum (TIBA) was used as such.

Isododecane was purified over aluminum oxide to reach a water content below 10 ppm.

A 101 g/L TIBA/isododecane solution was obtained by mixing the above components.

The melting points of the polymers (T_m) were measured by Differential Scanning Calorimetry (D.S.C.) on a Perkin Elmer DSC-7 instrument, according to the standard method. A weighted sample (5-7 mg) obtained from the polymerization was sealed into aluminum pans and heated to 180°C at 10°C/minute. The sample was kept at 180°C for 5 minutes to allow a complete melting of all the crystallites, then cooled to 20°C at 10°C/minute. After standing 2 minutes at 20°C, the sample was heated for the second time to 180°C at 10°C/min. In this second heating run, the peak temperature was taken as the melting temperature (T_m) and the area of the peak as melting enthalpy (ΔH_f).

Molecular weight parameters were measured using a Waters 150C ALC/GPC instrument (Waters, Milford, Massachusetts, USA) equipped with four mixed-gel columns PLgel 20 μ m Mixed-A LS (Polymer Laboratories, Church Stretton, United Kingdom). The dimensions of the columns were 300 \times 7.8 mm. The solvent used was TCB and the flow rate was kept at 1.0 mL/min. Solution concentrations were 0.1 g/dL in 1,2,4 trichlorobenzene (TCB). 0.1 g/L of 2,6- di-*t*-butyl-4-methyl phenol (BHT) was added to prevent degradation and the injection volume was 300 μ L. All the measurements were carried out at 135°C. GPC calibration is complex, as no well-characterized narrow molecular weight distribution standard reference materials are available for 1-hexene

polymers. Thus, a universal calibration curve was obtained using 12 polystyrene standard samples with molecular weights ranging from 580 to 13,200,000. It was assumed that the K values of the Mark-Houwink relationship were: $K_{PS} = 1.21 \times 10^{-4}$, dL/g and $K_{PH} = 1.78 \times 10^{-4}$ dL/g for polystyrene and poly-1-hexene respectively, for the copolymers the same K_{PH} has been used. The Mark-Houwink exponents α were assumed to be 0.706 for polystyrene and 0.725 for poly-1-hexene and copolymers. Even though, in this approach, the molecular parameters obtained were only an estimate of the hydrodynamic volume of each chain, they allowed a relative comparison to be made.

The intrinsic viscosity (I.V.) was measured in tetrahydronaphtalene (THN) at 135°C.

Rac dimethylsilyl{(2,4,7-trimethyl-1-indenyl)-7-(2,5-dimethyl-cyclopenta[1,2-b:4,3-b']-dithiophene)} zirconium dimethyl (A-1) was prepared according to the following procedure: the ligand, [3-(2,4,7-trimethylindenyl)][7-(2,5-dimethyl-cyclopenta[1,2-b:4,3-b']-dithiophene)]dimethyl silane, was prepared as described in WO 01/47939. 30.40 g of this ligand (72.26 mmol) and 170 ml of anhydrous THF were charged under nitrogen in a cylindrical glass reactor equipped with magnetic stirring bar. The brown solution so obtained was cooled and maintained at 0°C, while 58.4 ml of n-BuLi 2.5M in hexane (146 mmol) were added dropwise via dropping funnel. At the end of the addition, the dark brown solution was stirred for 1 hour at room temperature, then cooled to -50°C, and then 48.6 ml of MeLi 3.05 M in diethoxymethane (148.2 mmol) were added to it. In a Schlenk, 16.84 g of ZrCl₄ (72.26 mmol) were slurried in 170 ml of toluene. Both mixtures were kept at -50°C and the ZrCl₄ slurry was quickly added to the ligand dianion solution. At the end of the addition, the reaction mixture was allowed to reach room temperature and stirred for an additional hour. A yellow-green suspension was obtained. ¹H NMR analysis shows complete conversion to the target complex. All volatiles were removed under reduced pressure, and the obtained free flowing brown powder was suspended in 100 ml of Et₂O. After stirring for a few minutes, the suspension was filtered over a G4 frit. The solid on the frit was then washed twice with Et₂O (until the washing solvent turns from brown to yellow), then dried under vacuum, and finally extracted on the frit with warm toluene (60° C), until the filtering solution turns from yellow to colorless (about 650 ml of toluene); The extract was dried under reduced pressure to give 28.6 g of yellow powder, which ¹H-NMR showed to be the target complex, free from impurities. The yield based on the ligand was 73.3%.

¹H-NMR: (CD₂Cl₂, r.t.), ppm: -2.09 (s, 3H), -0.79 (s, 3H), 1.01(s, 3H), 1.04 (s, 3H), 2.38 (s, 3H), 2.39 (s, 3H), 2.43 (d, 3H, J = 1.37 Hz), 2.52 (s, 3H), 2.57 (d, 3 H, J = 1.37 Hz), 6.61(dq, 1 H, J = 7.04 Hz, J = 0.78 Hz), 6.81 (q, 1H, J = 1.37 Hz), 6.85 (dq, 1H, J = 7.04 Hz, J = 0.78 Hz), 6.87 (q, 1H, J = 1.37 Hz), 6.91 (s, 1H).

Flexural modulus, stress at break and elongation at break have been measured according to ISO 527-1 and ISO 178, Stress at yield and elongation at yield have been measured according to ASTM D 638, tensile modulus has been measured according to ASTM D 790, melt flow rate under the condition 230°C/2.16 kg is measured according to ISO 1133. Izod has been measured according to ASTM D256.

Preparation of catalyst systems

Preparation of catalyst system C-1

9.7 cc of TIBA/isododecane solution were mixed with 1.9cc of 30% MAO/toluene solution (MAO/TIBA, molar ratio 2:1). Then, 20 mg of A-1 were dissolved with this solution. The metallocene was completely soluble, the dark violet solution did not show any trace of residual solid. The final solution was obtained upon recovery of 2.0 cc by distillation. MAO/TIBA 2:1 mol/mol; Al_{tot}/Zr = 400. This solution was used to perform 1-hexene polymerization.

Polymerization tests

1-hexene homopolymerization, general procedure.

To 20g of liquid 1-hexene an amount of the catalyst solution obtained as reported above containing 0.5 mg of metallocene, is added at 50°C. After 30 minutes, the polymerization is stopped with ethanol. Then, acetone is added to separate the polymer. Finally, the polymer is dried at 50°C under vacuum for several hours. The results of the 1-hexene polymerization tests are reported in Table 1.

Table 1. 1-hexene polymerization results.

Ex	Cat.	Ageing, days	Yield, g	Activity Kg/g _{meth}
1	C-1	1	13.46	53.8

Preparation of catalyst system C-2 A1 /MAO:TIBA 2:1 (400)

33.3 ml of TIBA/isododecane solution (101g/L) was mixed with 7.9 cc of MAO/ toluene solution (Albemarle -30%wt) to obtain a MAO/TIBA molar ratio of 2:1. The solution was stirred for 1 hour at room temperature. Then, 69 mg of A-1 was dissolved in the solution.

The dark violet solution did not show any trace of residual solid.

The final solution was diluted with 13 ml of isododecane to reach a concentration of 100g/L.

1-hexene copolymerisation

An amount of liquid 1-hexene as indicated in table 2 were fed in a 250ml glass vessel reactor at room temperature. The reactor had been maintained under slight positive nitrogen atmosphere. Consequently the temperature was increased to the polymerization temperature indicated in table 2. An over pressure of 1 bar-g of propylene or 1-butene was fed in the autoclave. The catalyst solution, (ageing indicated in table 2), was transferred into the liquid, under a nitrogen flow. The pressure was increased with propylene until reaching the polymerisation pressure indicated in table 2. The polymerization was conducted for 60 minutes, then it was stopped by venting the monomers and the polymer was precipitated by adding acetone to the polymer solution. The recovered polymer was dried at 50°C under vacuum. Polymerization and polymer data are reported in table 2.

Table 2

Ex	Cat (mg. of A-1)	1- hexene g	Monomer (bar-g)	Pol. Temp. °C	Ageing hours	Activity Kg/g met/ h
2	C-2 (0.38)	67	propylene (3)	50	1	11
3	C-2 (0.38)	67	propylene (6)	50	4	32
4	C-2 (0.31)	40	1-butene (2)	50	450	30
5	C-2 (0.31)	40	1-butene (2)	70	450	43

Table 2 continued

Ex	1-hexene mol%	Mw	Mw/Mn	IV (THN) dl/g	ΔH
2	76.5	n.a.	n.a.	2.46	n.d.
3	58.5	n.a.	n.a.	2.53	n.d.
4	53.1	396371	2.2	3.20	n.d..
5	80.8	285718	1.9	1.33	n.d..

n.a. not available

n.d. not detectable

1-hexene/propylene or 1-butene copolymerisation

4 mmol of $\text{Al}(i\text{-Bu})_3$ (as a 1M solution in hexane) and 1000g of 1-hexene were charged at room temperature in a 4-L jacketed stainless-steel autoclave, previously purified by washing with an $\text{Al}(i\text{-Bu})_3$ solution in hexane and dried at 50°C in a stream of nitrogen. The autoclave was then thermostated at the polymerisation temperature, 70°C, and then the solution containing the catalyst/cocatalyst solution indicated in table 3 aged as indicated in table 3 was injected in the autoclave by means of nitrogen pressure through the stainless-steel vial. The monomer was fed until a pressure indicated in table 3 and the polymerisation carried out at constant temperature for 1 hour. The polymerization solution was discharged into a heated steel tank containing water at 70°C. The tank heating was switched off and a flow of nitrogen at 0.5 bar-g was fed. After cooling at room temperature, the steel tank was opened and the wet polymer collected and dried at 70°C under reduced pressure. The polymerisation conditions and the characterisation data of the obtained polymers are reported in Table 3.

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Table 3

Ex	Cat (mg. of A- 1)	Monomer (bar-g)	Activity Kg/g met/h	1-hexene mol%	Mw	Mw/Mn	IV (THN) dl/g	ΔH
6	C-2 (2.58)	propylene (20)	83	43	232200	1.9	1.4	n.d.
7	C-2 (1.28)	propylene (19)	117	20.7	229100	2.0	1.51	n.a.
8	C-2 (2.56)	1-butene (5)	20	41	217200	2.3	1.25	n.d.
9	C-2 (2.6)	Propylene (22)	148	46	217433	1.9	1.27	n.d.

The shore A (ISO 868) of copolymer of examples 6 and 8 has been measured, the results are reported in table 4. The tensile modulus of a sample of copolymers obtained in examples 6 and 8 has been measured according to (ASTM 5026, 4092 e 4065) as follows: Specimens for tensile test are cut from compression moulding plaques. Specimen sizes are approx. 40 mm long overall, 20 mm inter-clamp length, 6 mm width and thickness was 1 mm. Specimen is clamped in the SEIKO DMS 6100 tensile DMTA.

The applied frequency is 1 Hz.

Specimens are heated from -80°C to +140°C with 2°C/min as heating rate; specimens are re-clamped at the low temperature.

,The results are reported in table 4

Table 4

Ex	shore A	tensile modulus (MPa)
6	19	<10
8	7	<10

Blends

Samples of copolymers obtained in examples 6, 7 and 9 have been blended with Moplen^(T)HP500N a propylene homopolymer sold by Basell. three blends have been obtained by mixing in an extruder 20% of the copolymers of examples 6,7 and 8 and 80% of Moplen HP500N. The blends marked as BA (copolymer of example 6); BB (copolymer of example 7) and BC (copolymer of example) have been analyzed in order to evaluate the mechanical properties, the results are reported in table 5

Table 5

Blend		BC	BA	BB	HP500N
Melt flow rate	g/10min	13.1	13.1	14.3	1.8
Tensile modulus (DMTA) 23°C	MPa	1275	1130	1060	1450
Stress at yield	N/MM2	24.8	23.7	21.5	33
Elongation at yield	%	12.3	13	13.5	n.a.
Stress at break	N/MM2	16.6	15.4	12.6	n.a.
Elongation at break	%	70	65	60	n.a.
IZOD at 23°C	J/M	62.9	57.6	55	n.a.
IZOD at -20°C	J/M	17	18.5	17	n.a.

n.a. not available

It can be seen that the blend are much more softer than the homopolymer alone in fact, for example in the blend the tensile modulus is considerably lowered with respect to the homopolymer alone.

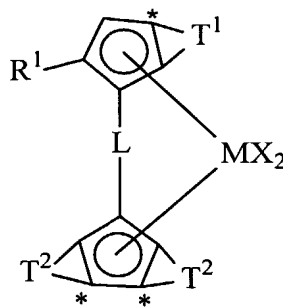
A blend of 8% of the copolymer obtained in example 6 and 82% of Hifax^(T) 7378 heterophasic blend comprising a crystalline matrix and a rubber phase sold by Basell has been obtained in a brandbury mixer. The resulting blend (BD) was analysed, the data are reported in table 6

Table 6

Blend		BD	Hifax 7378
Flexural modulus	MPa	1030	705
IZOD at 23°C	J/M	11.3	11.9
IZOD at -20°C	J/M	6.6	5.8

Claims

1. A process for preparing a polymer containing derived units of one or more alpha olefins of formula $\text{CH}_2=\text{CHW}$ wherein W is a $\text{C}_3\text{-C}_{10}$ hydrocarbon radical and optionally from 0 to 81% by mol of derived units of propylene or 1-butene, comprising contacting under polymerization conditions one or more alpha olefins of formula $\text{CH}_2=\text{CHW}$ and optionally propylene or 1-butene in the presence of a catalyst system obtainable by contacting:
 - a) a metallocene compound of formula (I)



(I)

wherein:

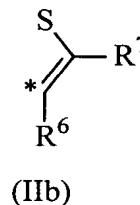
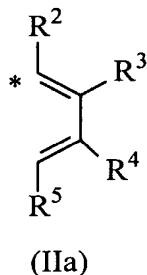
M is an atom of a transition metal selected from those belonging to group 3, 4, or to the lanthanide or actinide groups in the Periodic Table of the Elements;

X, same or different, is a hydrogen atom, a halogen atom, or a R, OR, OSO_2CF_3 , OCOR , SR, NR_2 or PR_2 group, wherein R is a are linear or branched, cyclic or acyclic, $\text{C}_1\text{-C}_{40}$ -alkyl, $\text{C}_2\text{-C}_{40}$ alkenyl, $\text{C}_2\text{-C}_{40}$ alkynyl, $\text{C}_6\text{-C}_{40}$ -aryl, $\text{C}_7\text{-C}_{40}$ -alkylaryl or $\text{C}_7\text{-C}_{40}$ -arylalkyl radicals; optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or two X can optionally form a substituted or unsubstituted butadienyl radical or a $\text{OR}'\text{O}$ group wherein R' is a divalent radical selected from $\text{C}_1\text{-C}_{40}$ alkylidene, $\text{C}_6\text{-C}_{40}$ arylidene, $\text{C}_7\text{-C}_{40}$ alkylarylidene and $\text{C}_7\text{-C}_{40}$ arylalkylidene radicals;

L is a divalent $\text{C}_1\text{-C}_{40}$ hydrocarbon radical optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements or a divalent silylene radical containing up to 5 silicon atom;

R^1 , is a hydrogen atom, or a $\text{C}_1\text{-C}_{40}$ hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements;

T^1 is a moiety of formula (IIa) or (IIb):

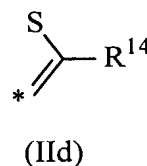
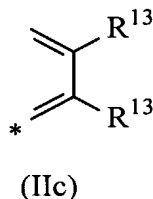


wherein the atom marked with the symbol * bonds the atom marked with the same symbol in the compound of formula (I);

R^2 , R^3 , R^4 and R^5 , equal to or different from each other, are hydrogen atoms, or C_1 - C_{40} hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or two adjacent R^2 , R^3 , R^4 and R^5 can optionally form a saturated or unsaturated, 5 or 6 membered rings, said ring can bear C_1 - C_{20} alkyl radicals as substituents;

R^6 and R^7 , equal to or different from each other, are hydrogen atoms or C_1 - C_{40} hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; or R^6 and R^7 can optionally form a saturated or unsaturated, 5 or 6 membered rings, said ring can bear C_1 - C_{20} alkyl radicals as substituents;

T^2 , equal to or different from each other, are moieties of formula (IIc) or (IId):



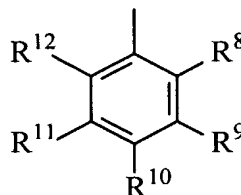
wherein the atom marked with the symbol * bonds the atom marked with the same symbol in the compound of formula (I);

R^{13} , equal to or different from each other, are hydrogen atoms or C_1 - C_{40} hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements;

R^{14} , equal to or different from each other, are hydrogen atoms or C_1 - C_{40} hydrocarbon radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; and

(b) an alumoxane or a compound capable of forming an alkyl metallocene cation;

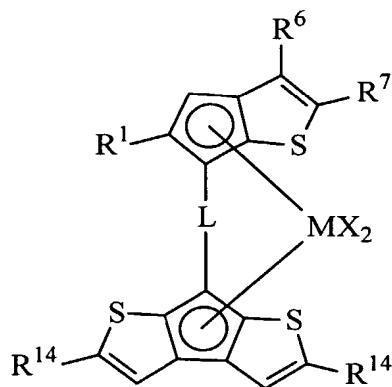
2. The process according to claim 1 wherein the catalyst system further contains c) an organo aluminum compound.
3. The process according to claims 1 or 2 wherein in the compound of formula (I) M is titanium, zirconium or hafnium; X is a hydrogen atom, a halogen atom or a R group, wherein R has been defined as in claim 1; and L is a divalent bridging group selected from C₁-C₄₀ alkylidene, C₃-C₄₀ cycloalkylidene, C₆-C₄₀ arylidene, C₇-C₄₀ alkylarylidene, or C₇-C₄₀ arylalkylidene radicals optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements, and silylene radical containing up to 5 silicon atoms.
4. The process according to anyone of claims 1-3 wherein in the compound of formula (I) L is a group (Z(R''))₂_n wherein Z is a carbon or a silicon atom, n is 1 or 2 and R'' is a C₁-C₂₀ hydrocarbon radical optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements.
5. The process according to anyone of claims 1-4 wherein in the compound of formula (I) R¹ is linear or branched, saturated or unsaturated C₁-C₂₀-alkyl radicals, optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; R² is a linear or branched, saturated or unsaturated C₁-C₂₀-alkyl radical, optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; R⁴ is a hydrogen atom or a C₁-C₁₀-alkyl radical; R⁵ is preferably a hydrogen atom or linear or branched, saturated or unsaturated C₁-C₂₀-alkyl radical, optionally containing heteroatoms belonging to groups 13-17 of the Periodic Table of the Elements; R⁷ is a hydrogen atom or a linear or branched, cyclic or acyclic C₁-C₂₀-alkyl radical;
R⁶ is a group of formula (III)



(III)

wherein R⁸, R⁹, R¹⁰, R¹¹ and R¹², equal to or different from each other, are hydrogen atoms or C₁-C₂₀ hydrocarbon radicals.

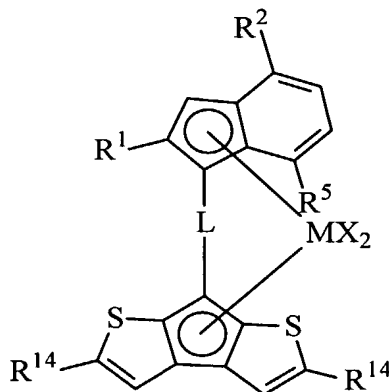
6. The process according to anyone of claims 1-5 wherein in the compound of formula (I) has formula (IV)



(IV)

wherein M, X, L, R¹, R⁶, R⁷ and R¹⁴ are described in claim 1.

7. The process according to anyone of claims 1-5 wherein in the compound of formula (I) has formula (V)



(V)

wherein M, X, L, R¹, R², R⁵ and R¹⁴ are described in claim 1.

8. The process according to anyone of claims 1-7 wherein the polymerization process is carried out by using 1-hexene as polymerization medium.
9. The process according to anyone of claims 1-8 wherein 1-hexene is polymerized.
10. The process according to anyone of claims 1-8 wherein 1-hexene is copolymerized with propylene or 1-butene.
11. A copolymer comprising from 41% by mol to 99.9% by mol of derived units of alpha olefins of formula CH₂=CHW wherein W is a C₃-C₁₀ hydrocarbon radical and from 0.1 to 59% by mol of derived units of propylene or 1-butene endowed with the following properties:

- i) intrinsic viscosity IV measured tetrahydronaphtalene (THN) at 135°C higher than 0.90 dl/g;
 - ii) distribution of molecular weight Mw/Mn lower than 3; and
 - iii) no enthalpy of fusion detectable at a differential scanning calorimeter (DSC) wherein the DSC measurement is carried out as described below.
12. A copolymer according to claim 11 endowed with a shore A lower than 30 and a tensile modulus lower than 20 MPa.
13. A blend comprising the copolymer of claims 11 or 12.
14. Use of the copolymer of claims 11 and 12 as compatibilizer in an heterophasic blend comprising a crystalline matrix and a rubber phase.

INTERNATIONAL SEARCH REPORT

International Application No
PCT/EP2005/002481

A. CLASSIFICATION OF SUBJECT MATTER
IPC 7 C08F210/14

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 7 C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, CHEM ABS Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 01/47939 A (BASELL TECHNOLOGY COMPANY B.V; NIFANT'EV, ILYA, E; GUIDOTTI, SIMONA; R) 5 July 2001 (2001-07-05) cited in the application the whole document	1-10
X	EP 0 604 908 A (BASELL TECHNOLOGY COMPANY B.V; SPHERILENE S.R.L) 6 July 1994 (1994-07-06) example 20	11-14
X	GB 999 725 A (EASTMAN KODAK COMPANY) 28 July 1965 (1965-07-28) the whole document	11-14
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INTERNATIONAL SEARCH REPORT

International Application No
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